

***Centro Interdipartimentale
per la Ricerca Applicata e i Servizi
nel Settore della Meccanica Avanzata e della Motoristica***



Unità Operativa di Ricerca 1.4

Laboratorio di tecniche antincendio per l'industria meccanica

Responsabile

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FIRE PROTECTION

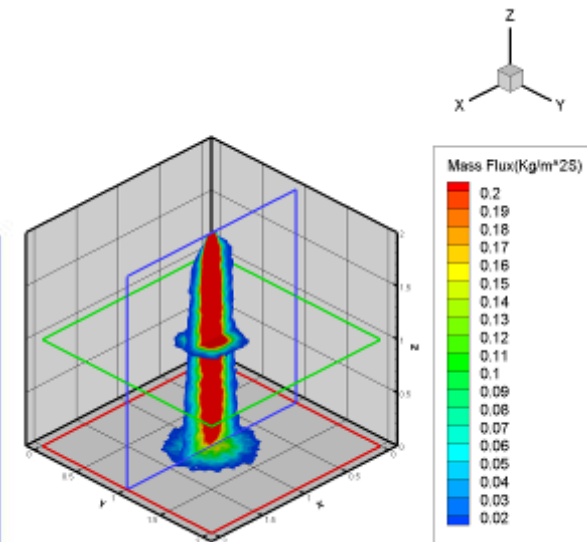
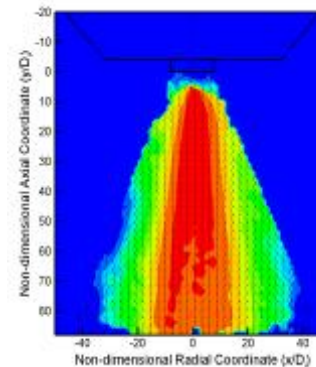
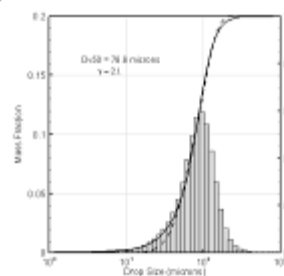
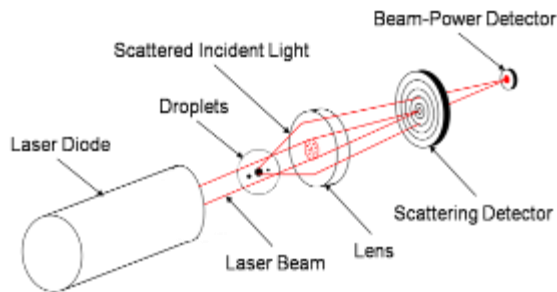
Water Mist Systems

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Discharge and dispersion analysis of water mist sprays

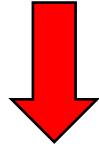
Characterization of the atomization process of a water jet exiting a high-pressure single injector :

- laser-based experimental device
- data on the drop size distribution are collected by experiments at high pressure (80 bar)
- a theoretical model has been developed to predict velocity at the injector outlet
- CFD predictions by FDS code are carried out for the distribution of mass flux at different heights from the outlet



INTRODUCTION AND FOCUS

WATER MIST



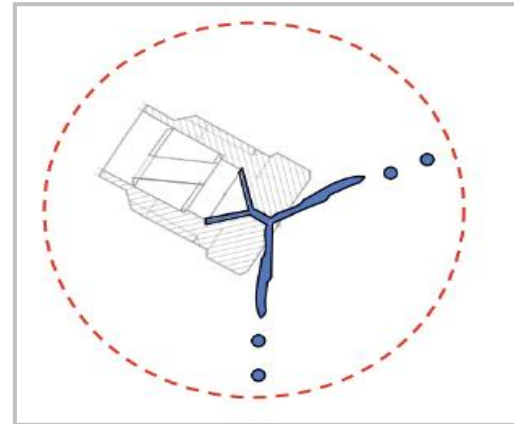
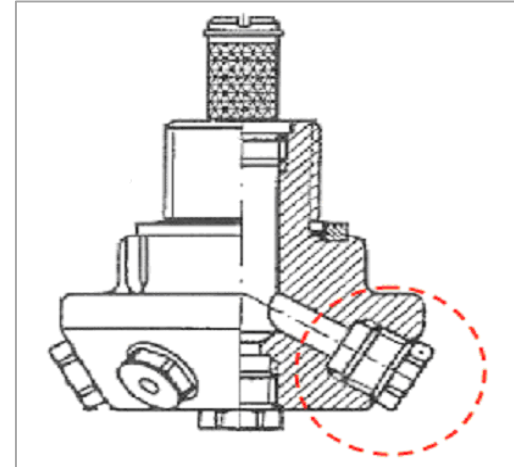
SMALL DROP SIZE
($D_{v50} < 100 \mu\text{m}$)



HIGH PRESSURE (> 35 bar)
NOZZLES

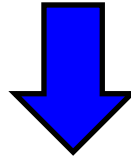


NEED FOR SPRAY
CHARACTERIZATION
(Nozzle design, CFD modeling, etc.)



SPRAY CHARACTERIZATION: AREAS OF INVESTIGATION; PARAMETERS OF INTEREST

ATOMIZATION & DISPERSION



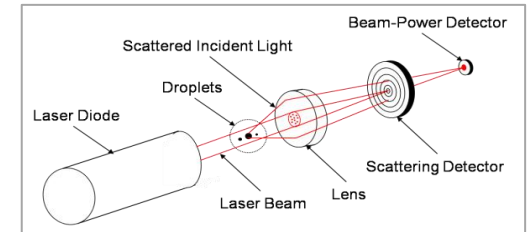
- DROP SIZE & MASS FLUX DISTRIBUTION
- INITIAL VELOCITY
- SPRAY CONE ANGLE

PRESSURE RANGE FOR THE EXPERIMENTAL TESTS:
50 - 90 bar

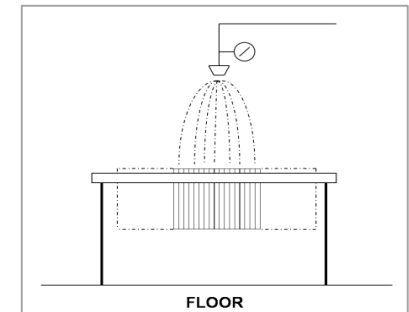
EXPERIMENTAL TESTS: MEASUREMENT TECHNIQUES AND INSTRUMENTS

- Drop Size

Malvern Spraytec

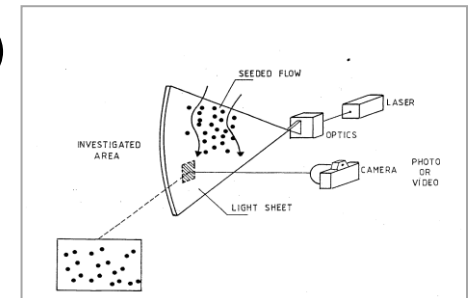


- Mass-Flux Distribution Mechanical Patternator



- Initial Velocity

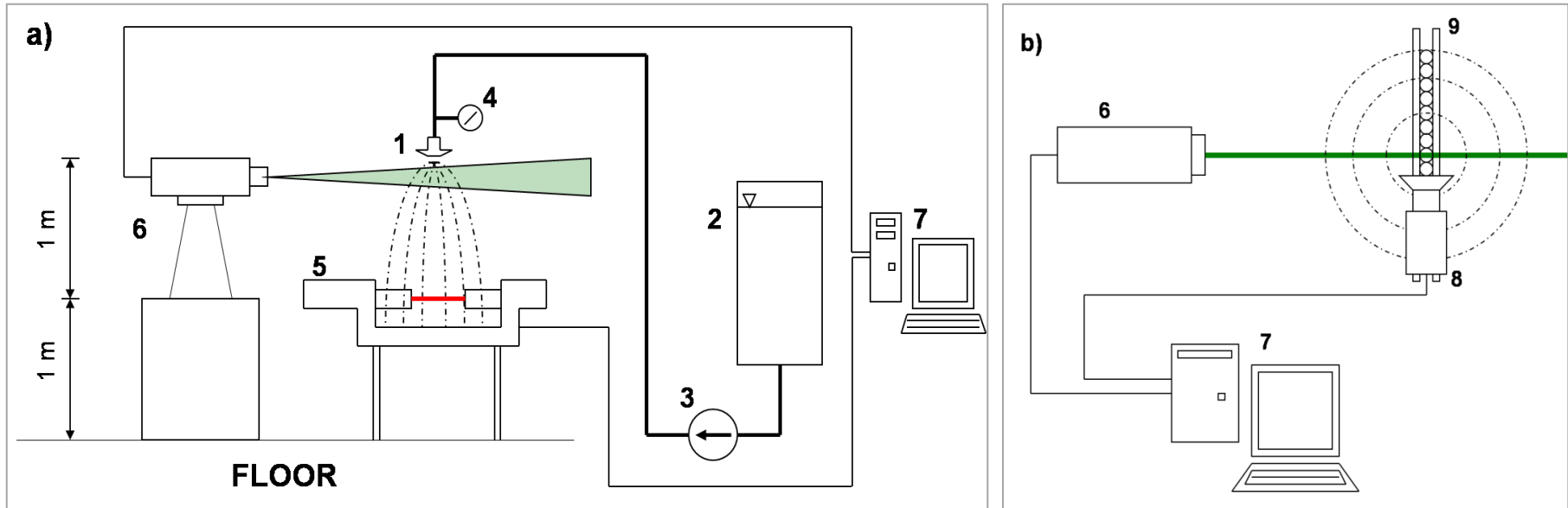
Particle Image Velocimetry (PIV)



- Spray Cone Angle

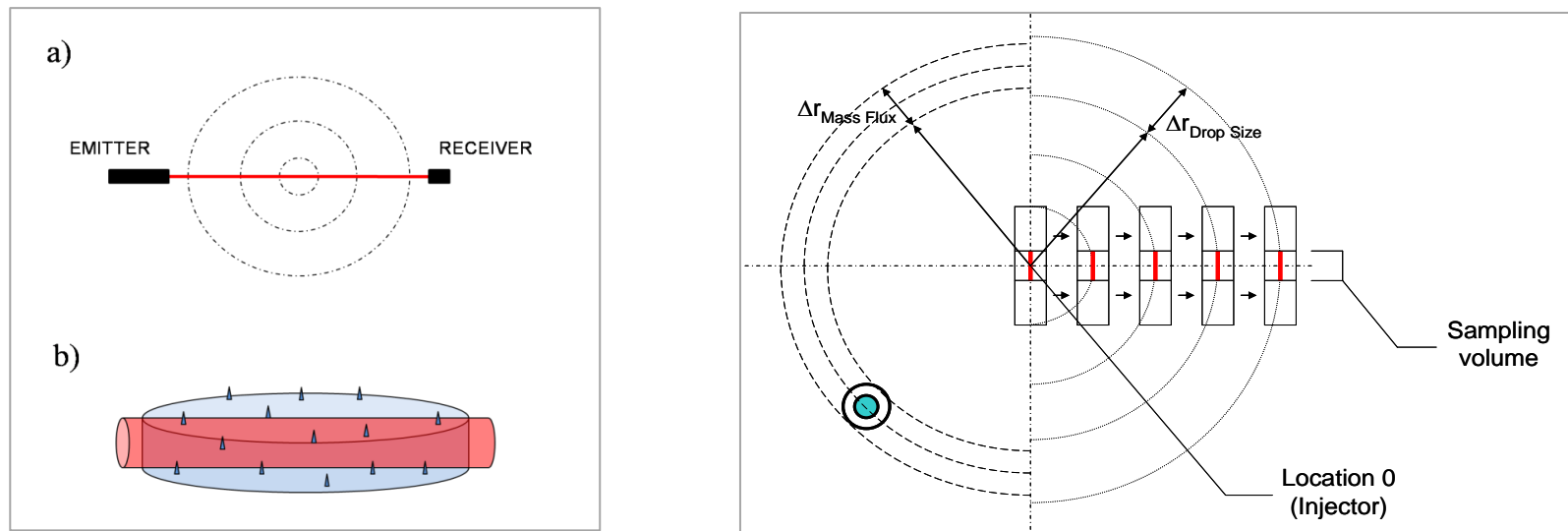
PIV Maps / Velocity Profiles

EXPERIMENTAL FACILITY



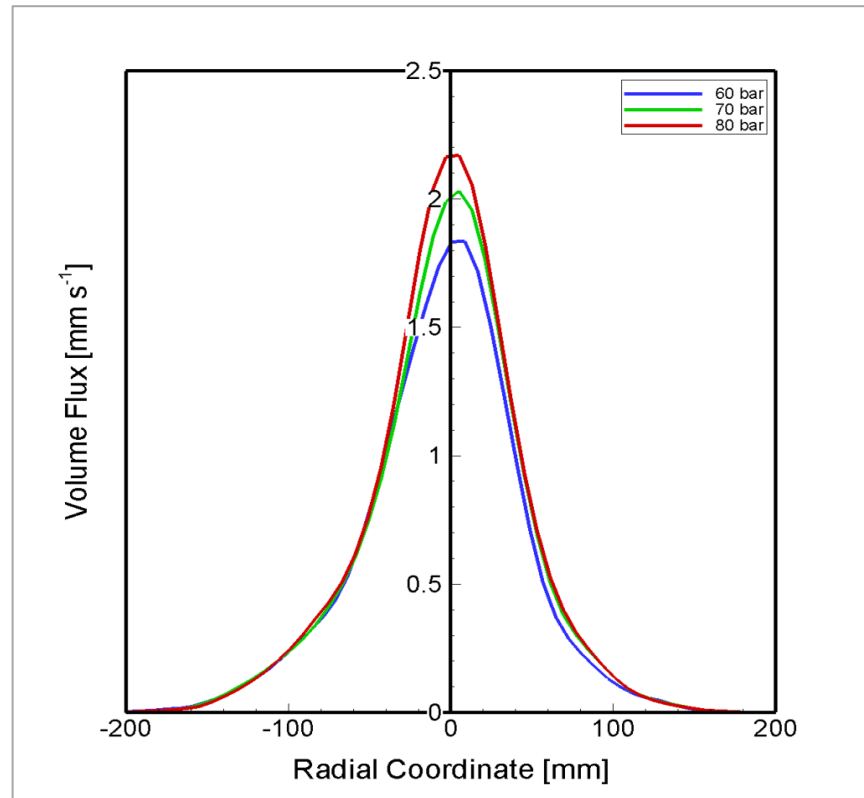
Sketch of the experimental facility. a) view from side: 1. Nozzle, 2. Tank, 3. Electric Pump, 4. Pressure Gauge, 5. *Malvern Spraytec*, 6. PIV Laser Emitter, 7. Data-Acquisition System; b) view from above: 8. PIV CCD Camera, 9. Mechanical Patternator.

DROP-SIZE AND MASS-FLUX MEASUREMENT: METHODOLOGY



Drop-size measurements are weighted through mass-flux distribution. Raw results given by *Malvern Spraytec* are biased because of the mismatch between the shape of the laser beam (sampling volume) and the shape of a spray section. Hypothesis of radial symmetry has been applied.

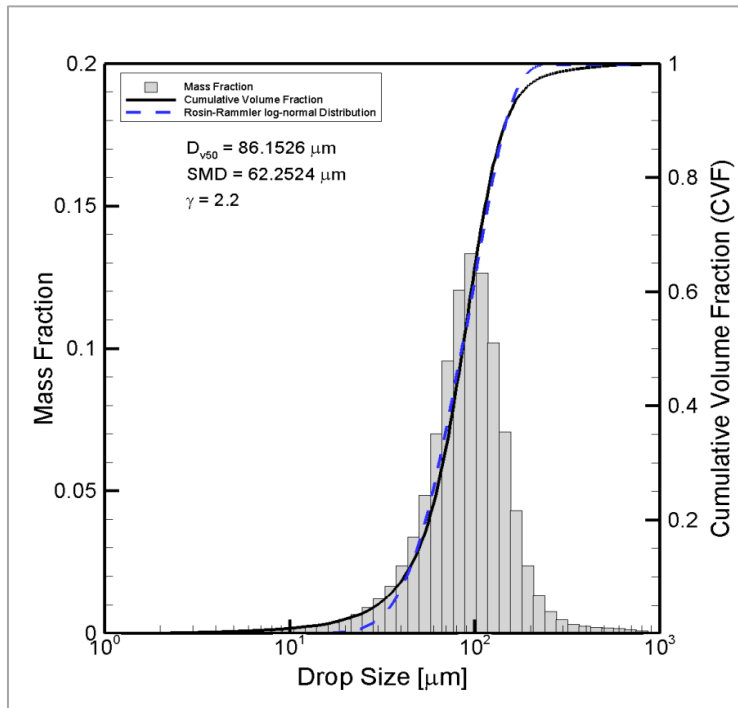
MASS-FLUX DISTRIBUTION: EXPERIMENTAL RESULTS



The radial coordinate has been reconstructed setting the center of mass as the 0 point (*real 0*). It is not perfectly coincident with the geometric 0 point because of little experimental asymmetries (distance lower than 18 mm).

DROP-SIZE RECONSTRUCTION

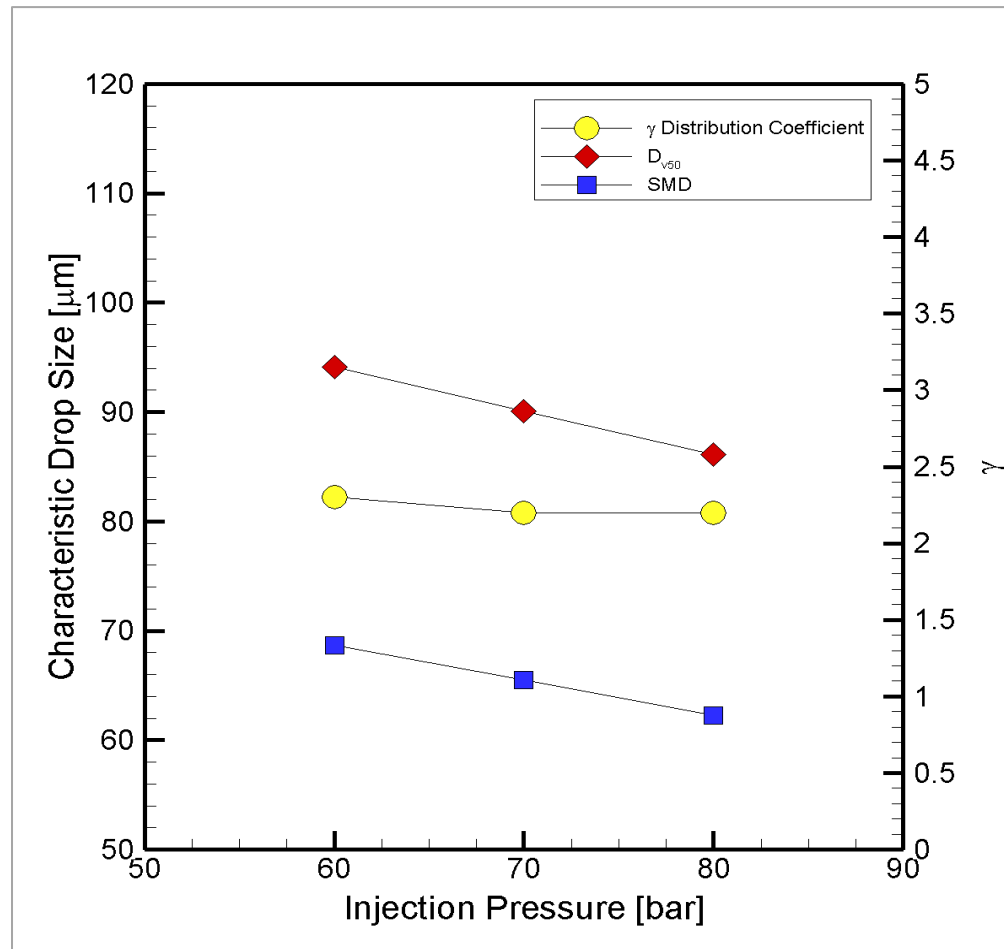
- Volume-flux distribution has been mirrored with respect to y axis;
- A polynomial curve has been employed to fit the obtained points;
- Drop-size data have been averaged over mass-flux curve to reconstruct the experimental CVF (Cumulative Volume Fraction) vs. Drop Size curve.



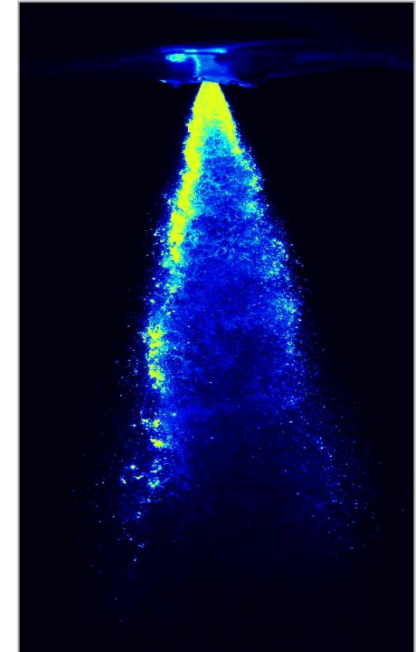
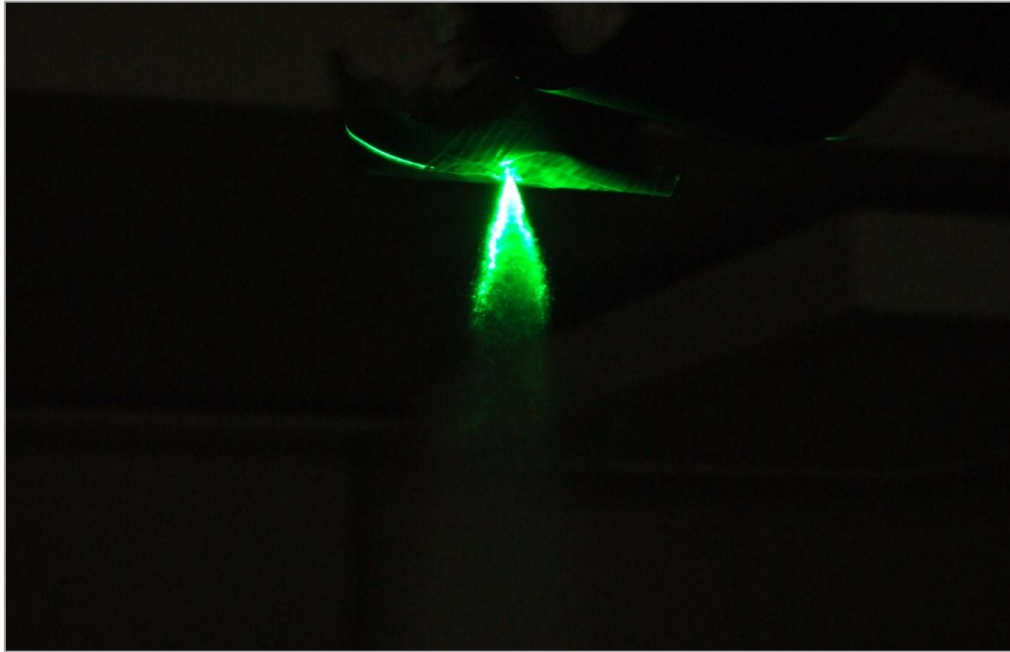
Rosin-Rammler Log-Normal Distribution

$$CVF = \begin{cases} (2\pi)^{-1/2} \int_0^{D_{CVF}} (\gamma' D)^{-1} e^{-\frac{[\ln(D/D_{v50})]^2}{2\gamma'^2}} dD & (D_{CVF} \leq D_{v50}) \\ 1 - e^{-0.693(D_{CVF}/D_{v50})^\gamma} & (D_{v50} < D_{CVF}) \end{cases}$$

DROP SIZE: EXPERIMENTAL RESULTS

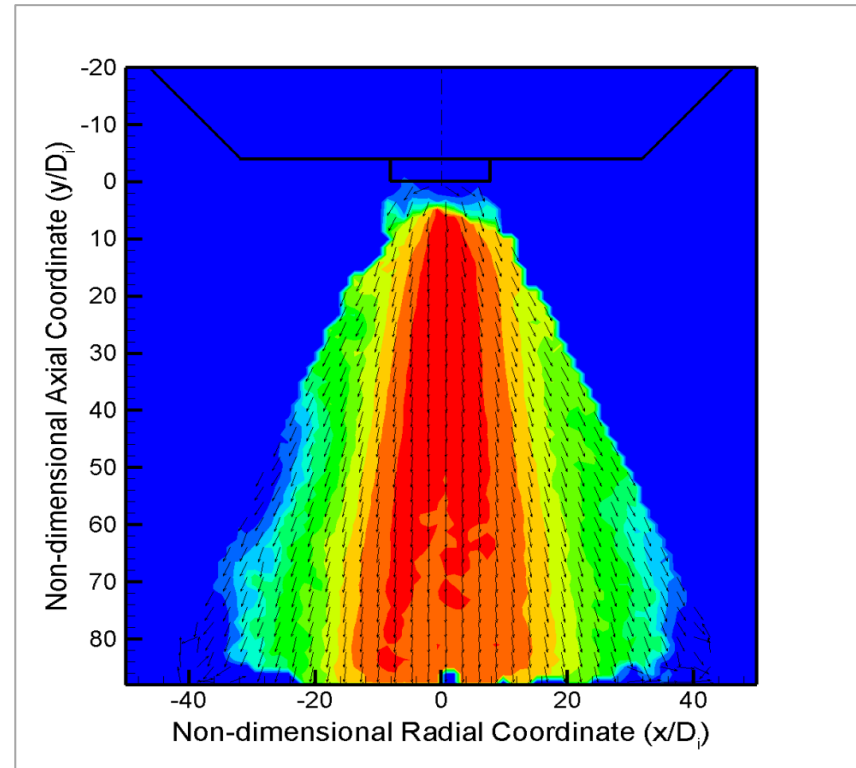
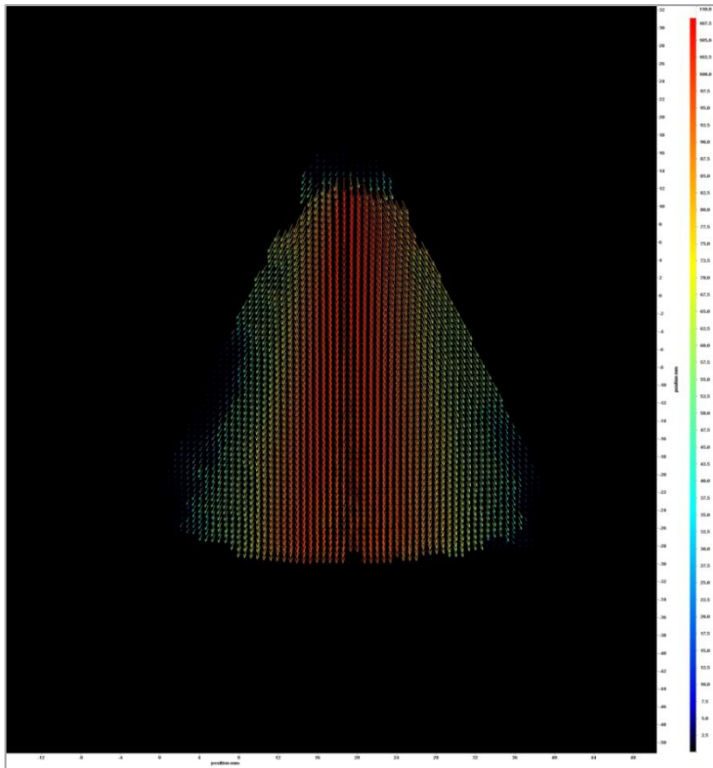


PIV VISUALIZATION OF INITIAL SPRAY



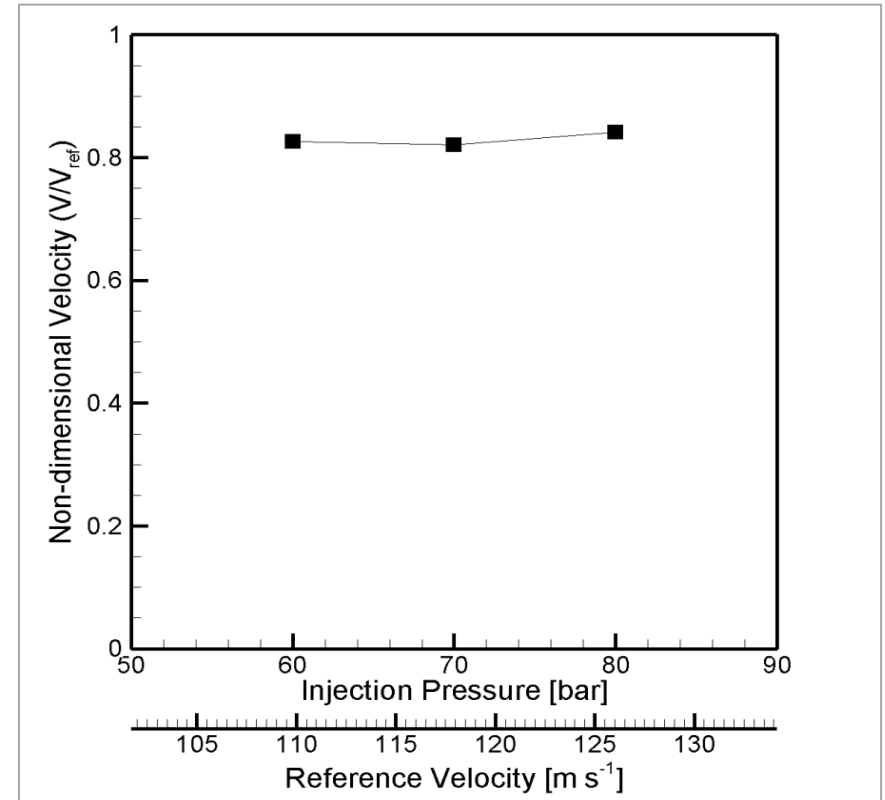
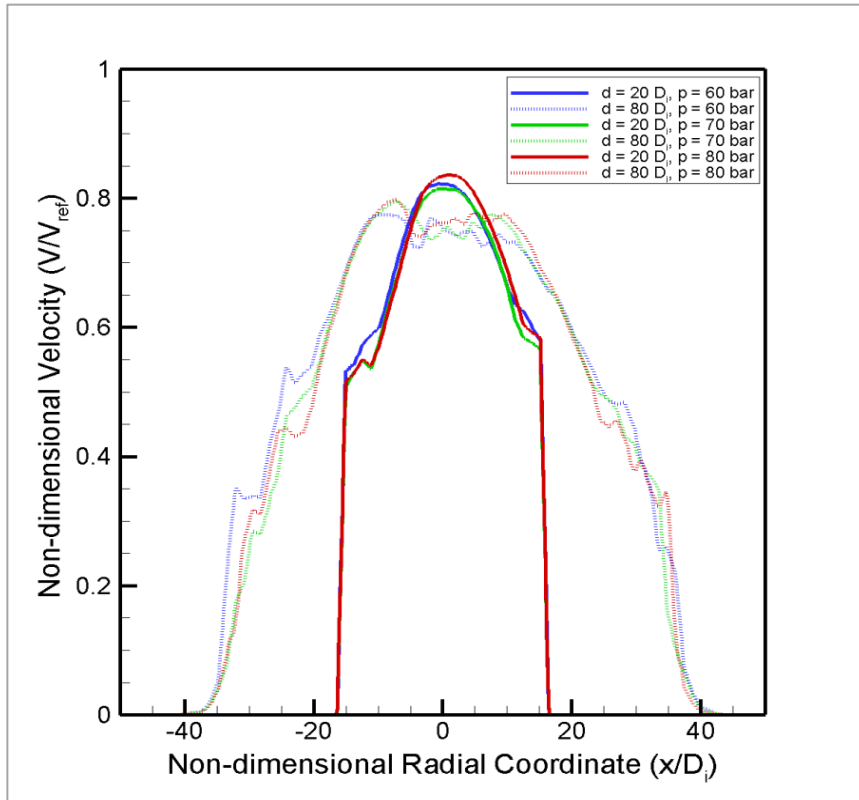
- No seeding particles have been added: droplets are tracking particles themselves.
- Initial velocity has been measured only on the plane containing the injector axis, because tangential component becomes negligible after about 5 mm along the axis.
- Breakup occurs in the first 2 mm; the investigation region covers the first 40 mm.

PIV MAPS OF THE INITIAL SPRAY



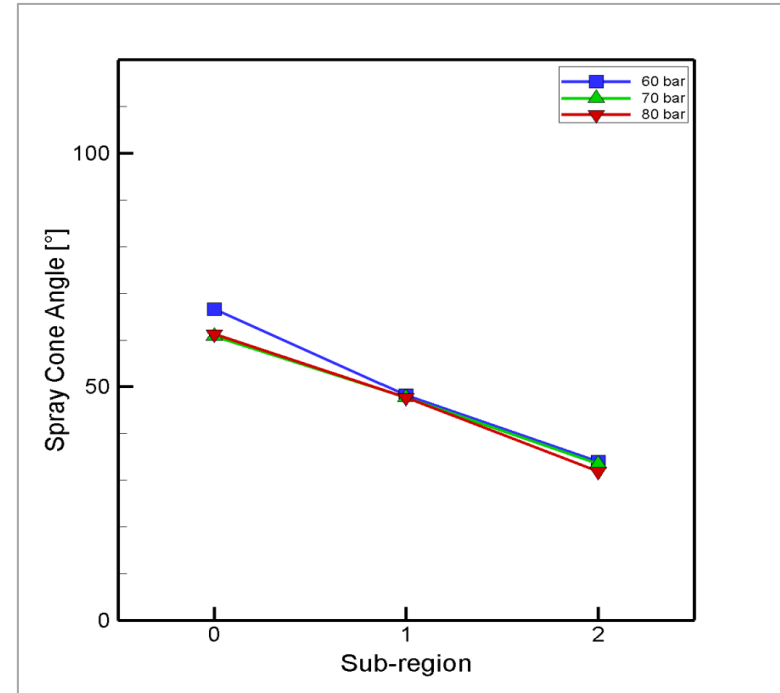
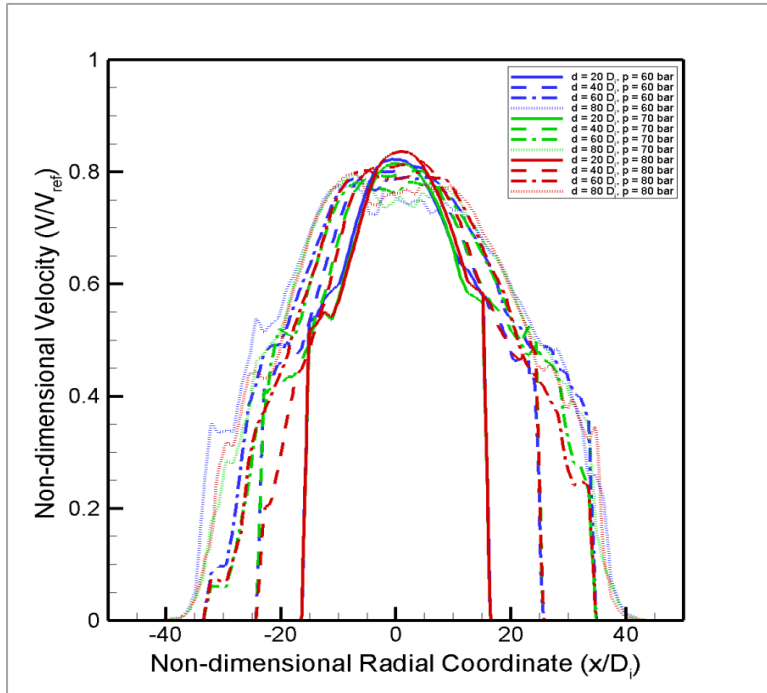
Velocity vectors and contours at 80 bar

INITIAL VELOCITY: EXPERIMENTAL RESULTS

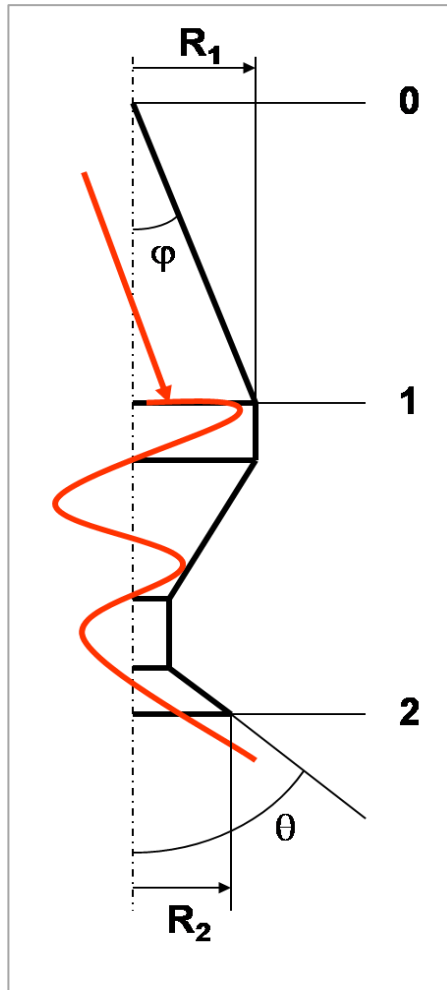


Radial velocity profiles along the injector axis and initial velocity magnitude

EVALUATION OF SPRAY-CONE ANGLE



PHYSICAL MODEL – PREDICTIVE CORRELATION



An inviscid model (Bernoulli model) has been developed following a classical approach to pressure-swirl atomizers (Lefebvre, 1989).

$$V_2 = \left(\frac{2p_{PG}}{\rho_L} \right)^{1/2}$$

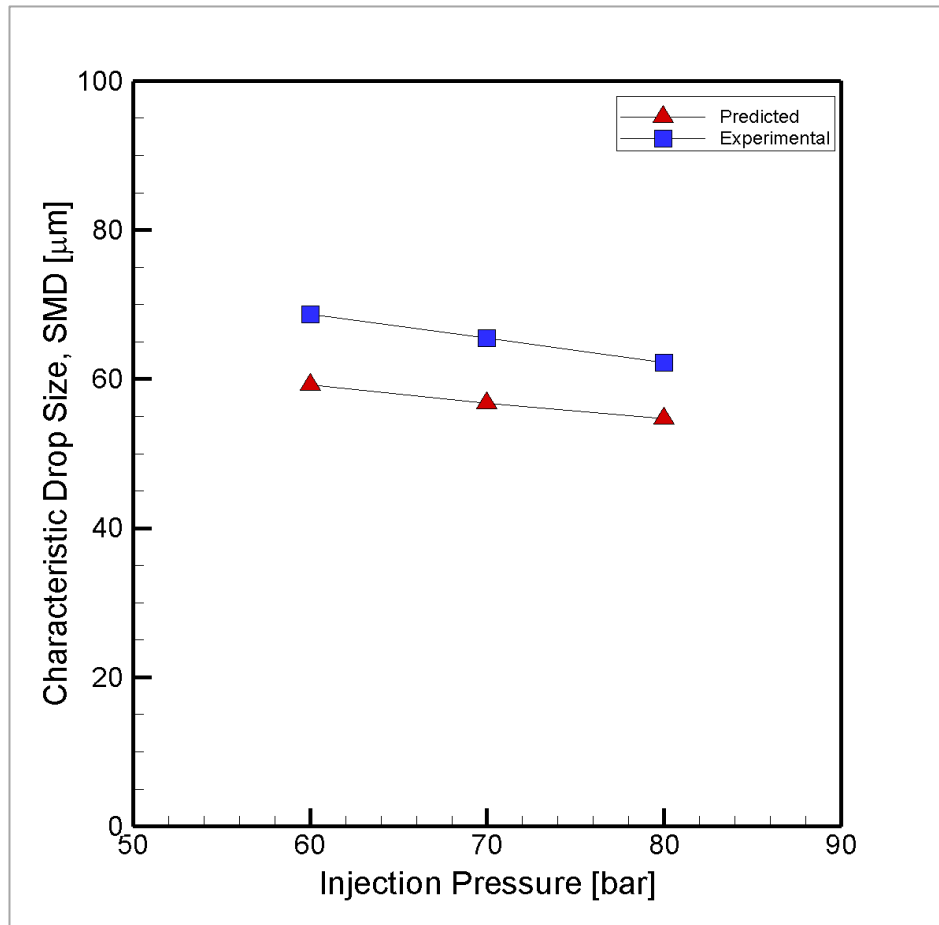
$$\dot{m}_L = \rho_L A_F V_2 = \rho_L C_D A_{TOT} V_2 = C_D A_{TOT} (2\rho_L p_{PG})^{1/2}$$

$$C_D = \frac{FN}{A_{TOT}} \left(\frac{\rho_L}{2} \right)^{1/2}$$

Radcliffe's correlation

$$SMD = 7.3 \cdot \sigma^{0.6} \cdot \nu^{0.2} \cdot \dot{m}_L^{0.25} \cdot p_L^{-0.4}$$

COMPARISON BETWEEN EXPERIMENTAL AND THEORETICAL RESULTS





In collaboration with

